CLAIM AMENDMENTS

Amended claims: 1-12 and added new claims 13-22.

1. (Currently Amended) A process ~~Process~~ to prepare a haze free base oil having a kinematic viscosity at 100 °C of greater than 10 cSt from a Fischer-Tropsch wax feed ~~by performing~~ comprising the following steps[[,]]:

(a) reducing the wax content of a Fischer-Tropsch wax ~~the~~ feed by contacting the feed with a hydroisomerisation catalyst under hydroisomerisation conditions at a remote location to form an intermediate product[[,]];

(b) transporting ~~an~~ the intermediate product having the reduced wax content as obtained in step (a) from ~~one~~ the remote location to another location closer to the end-user [[,]]; and

(c) solvent dewaxing the transported intermediate product to obtain ~~the~~ a haze free base oil at the location closer to the end-user.

2. (Currently Amended) The process ~~Process~~ according to claim 1, wherein the feed to step (a) has a 10 wt% recovery boiling point of above 500 °C and a wax content of greater than 50 wt%.

3. (Currently Amended) The process according to claim 2, wherein the wax content in the feed is between 60 and 95 wt%.

4. (Currently Amended) The process according to claim 2, ~~Process according to any one of claims 2-3,~~ wherein the 10 wt% recovery boiling point of the feed is between 500 and 550 °C.

5. (Currently Amended) The process according to claim 1, ~~Process according to any one of claims 1-4,~~ wherein the wax content in the intermediate product is between 10 and 35 wt%.

6. (Currently Amended) The process according to claim 1, ~~Process according to any one of claims 1-5~~, wherein the intermediate product has a congealing point of between 20 and 60 °C.

7. (Currently Amended) The process according to claim 1, ~~Process according to any one of steps 1-6,~~ wherein more than 50 wt% of the intermediate product boils above the 10 wt% recovery point of the feed used in step (a).

8. (Currently Amended) The process ~~Process~~ according to claim 7, wherein more than 70 wt% of the intermediate product boils above the 10 wt% recovery point of the feed used in step (a).

9. (Currently Amended) The process according to claim 1, ~~Process according to any one of claims 1-8,~~ wherein the hydroisomerisation catalyst used in step (a) is a substantially amorphous based catalyst comprising a silica-alumina carrier and a noble or non-noble Group VIII metal.

10. (Currently Amended) The process according to claim 1, ~~Process according to any one of claims 1-8,~~ wherein the hydroisomerisation catalyst used in step (a) is a molecular sieve based catalyst and a noble or non-noble Group VIII metal.

11. (Currently Amended) The process according to claim 1, ~~Process according to any one of claims 1-10,~~ wherein step (b) is performed by means of a ship and wherein ~~the ships~~ containers on the ship are firsted purged with nitrogen before loading and wherein the nitrogen is obtained in an air-separation unit which unit also isolates oxygen for use to make syngas which in turn is used as feedstock to prepare the Fischer-Tropsch wax feed.

12. (Currently Amended) A process ~~Process~~ to prepare a lubricant composition not containing a viscosity modifier additive by blending a low viscosity base oil with ~~the~~ a haze free base oil ~~as obtained in step (c) of the process as described in claims 1-11 and one or more additives~~ having a kinematic viscosity at 100°C of greater than 10 cSt from a Fischer-Tropsch wax feed prepared by a process comprising the following steps:

(a) reducing the wax content of a Fischer-Tropsch wax feed by contacting the feed with a hydroisomerisation catalyst under hydroisomerisation conditions at a remote location to form an intermediate product;

(b) transporting the intermediate product having the reduced wax content as obtained in step (a) from the remote location to another location closer to the end-user; and

(c) solvent dewaxing the transported intermediate product to obtain a haze free base oil at the location closer to the end-user.

13. (New) The process according to claim 12, wherein the feed to step (a) has a 10 wt% recovery boiling point of above 500 °C and a wax content of greater than 50 wt%.

14. (New) The process according to claim 12, wherein the wax content in the feed is between 60 and 95 wt%.

15. (New) The process according to claim 12, wherein the 10 wt% recovery boiling point of the feed is between 500 and 550 °C.

16. (New) The process according to claim 12, wherein the wax content in the intermediate product is between 10 and 35 wt%.

17. (New) The process according to claim 12, wherein the intermediate product has a congealing point of between 20 and 60 °C.

18. (New) The process according to claim 12, wherein more than 50 wt% of the intermediate product boils above the 10 wt% recovery point of the feed used in step (a).

19. (New) The process according to claim 12, wherein more than 70 wt% of the intermediate product boils above the 10 wt% recovery point of the feed used in step (a).

20. (New) The process according to claim 12, wherein the hydroisomerisation catalyst used in step (a) is a substantially amorphous based catalyst comprising a silica-alumina carrier and a noble or non-noble Group VIII metal.

21. (New) The process according to claim 12, wherein the hydroisomerisation catalyst used in step (a) is a molecular sieve based catalyst and a noble or non-noble Group VIII metal.

22. (New) The process according to claim 12, wherein step (b) is performed by means of a ship and wherein containers on the ship are first purged with nitrogen before loading and wherein the nitrogen is obtained in an air-separation unit which unit also isolates oxygen for use to make syngas which in turn is used as feedstock to prepare the Fischer-Tropsch wax feed.